F25J  LIQUEFACTION, SOLIDIFICATION OR SEPARATION OF GASES OR GASEOUS MIXTURES BY PRESSURE AND COLD TREATMENT (OR LIQUEFIED GASEOUS) MIXTURES BY PRESSURE AND COLD TREATMENT (OR BY BRINGING THEM INTO THE SUPERCRITICAL STATE (cryogenic pumps F04B 37/08; gas storage vessels, gas holders F17; filing vessels with, or discharging from vessels, compressed, liquefied or solidified gases F17C; refrigeration machines, plants, or systems F25B))

WARNING
In this subclass non-limiting references (in the sense of paragraph 39 of the Guide to the IPC) may still be displayed in the scheme.

1/00 Processes or apparatus for liquefying or solidifying gases or gaseous mixtures (recovering volatile solvents by condensation B01D 5/00; vapor recovery systems combined with filling nozzles B67D 7/54; solidification of carbonic acid C01B 32/55; for ammonia in general C01C 1/00)
  1/0002 . . . [characterised by the fluid to be liquefied]
  1/0005 . . . [Light or noble gases (F25J 1/0012 takes precedence)]
  1/0007 . . . [Helium]
  1/001 . . . [Hydrogen]
  1/0012 . . . [Primary atmospheric gases, e.g. air]
  1/0015 . . . [Nitrogen]
  1/0017 . . . [Oxygen]
  1/002 . . . [Argon]
  1/0022 . . . [Hydrocarbons, e.g. natural gas]
  1/0025 . . . [Boil-off gases "BOG" from storages]
  1/0027 . . . [Oxides of carbon, e.g. CO₂]
  1/003 . . . [characterised by the kind of cold generation within the liquefaction unit for compensating heat leaks and liquid production]
  1/0032 . . . [using the feed stream itself or separated fractions from it, i.e. "internal refrigeration"]
  1/0035 . . . [by gas expansion with extraction of work]
  1/0037 . . . [of a return stream]
  1/004 . . . [by flash gas recovery (F25J 1/0027 takes precedence)]
  1/0042 . . . [by liquid expansion with extraction of work]
  1/0045 . . . [by vaporising a liquid return stream]
  1/0047 . . . [using an "external" refrigerant stream in a closed vapor compression cycle (F25J 1/0021, F25J 1/0025 take precedence)]
  1/005 . . . [by expansion of a gaseous refrigerant stream with extraction of work]
  1/0052 . . . [by vaporising a liquid refrigerant stream]
  1/0055 . . . [originating from an incorporated cascade]
processes treating not the same feed stream

{Coupling of the liquefaction unit to other units provided before, e.g. heat driven absorption using other external refrigeration means not using the cold stored in an external cryogenic component in an open refrigeration loop}

{integration with an intermediate heat exchange fluid between the cryogenic component and the fluid to be liquefied (F25J 1/0224 takes precedence)}

{combination with the subsequent re-vaporisation of the originally liquefied gas at a second location to produce the external cryogenic component}

{integration with an internal quasi-closed refrigeration loop, e.g. using a deep flash recycle loop}

{using the cold stored in an external cryogenic component in an open refrigeration loop}

{within a refrigeration cascade}

{Coupling of the liquefaction unit to other units or processes, so-called integrated processes (combined plants, e.g. engine plant combined with an industrial process F01K 23/064: gas turbine plants in combination with other processes F02C 6/00)}

{Integration with a unit for using hydrocarbons, e.g. consuming hydrocarbons as feed stock}

{for the combustion as fuels, i.e. integration with the fuel gas system}

{for the working-up of the hydrocarbon feed, e.g. reinjection of heavier hydrocarbons into the liquefied gas}

{integration within a pressure letdown station of a high pressure pipeline system}

{Integration with a cryogenic air separation unit (cryogenic separation of air F25J 3/043)}

{Heat exchange integration}

{providing refrigeration for different processes treating not the same feed stream}

{integrating refrigeration provided for liquefaction and purification/treatment of the gas to be liquefied, e.g. heavy hydrocarbon removal from natural gas (details related to rectification F25J 3/021; details related to partial condensation F25J 3/006; working-up natural gas C10L 3/10)}

{Purification or treatment step is integrated within one refrigeration cycle only, i.e. the same or single refrigeration cycle provides feed gas cooling (if present) and overhead gas cooling}

{Purification or treatment step being integrated between two refrigeration cycles of a refrigeration cascade, i.e. first cycle providing feed gas cooling and second cycle providing overhead gas cooling}

{wherein the overhead cooling comprises providing reflux for a fractionation step}

{Waste heat recovery, e.g. from heat of compression}

{Start-up or control of the process; Details of the apparatus used; Details of the refrigeration compression system used}

{Operation; Control and regulation; Instrumentation (F25J 1/0279 takes precedence)}

{Different modes, i.e. 'runs', of operation; Process control}

{start-up of the process}

{Stopping of the process, e.g. defrosting or deriming, maintenance; Back-up mode or systems}

{Controlling refrigerant inventory, i.e. composition or quantity (charging or discharging refrigerants in cooling systems F25B 45/00)}

{Details related to the refrigerant production or treatment, e.g. make-up supply from feed gas itself}

{Intermittent or alternating process, so-called batch process, e.g. "peak-shaving"}

{Control strategy, e.g. advanced process control or dynamic modeling}

{controlling particular process parameter, e.g. pressure, temperature}

{controlling the composition of the feed or liquefied gas, e.g. to achieve a particular heating value of natural gas}

{Safety aspects of operation (F25J 1/0298 takes precedence)}

{Construction and layout of liquefaction equipments, e.g. valves, machines (F25J 1/0279 takes precedence)}

{vertical layout of the equipments within in the cold box}

{Modularity and arrangement of parts of the liquefaction unit and in particular of the cold box, e.g. pre-fabrication, assembling and erection, dimensions, horizontal layout "plot"
F25J

1/0261 . . . . {Details of cold box insulation, housing and internal structure (buildings forming parts of cooling plants C04H 5/10)}
1/0262 . . . . {Details of the cold heat exchange system (constructional details F25J 5/00, construction of cold-exchangers in general F28)}
1/0263 . . . . {using different types of heat exchangers}
1/0264 . . . . {Arrangement of heat exchanger cores in parallel with different functions, e.g. different cooling streams (F25J 1/0272 takes precedence)}
1/0265 . . . . {comprising cores associated exclusively with the cooling of a refrigerant stream, e.g. for auto-refrigeration or economizer}
1/0267 . . . . {using flash gas as heat sink}
1/0268 . . . . {using a dedicated refrigeration means (F25J 1/0296 takes precedence)}
1/0269 . . . . {Arrangement of liquefaction units or equipments fulfilling the same process step, e.g. multiple "trains" concept (F25J 1/0294 takes precedence)}
1/027 . . . . {Inter-connecting multiple hot equipments upstream of the cold box}
1/0271 . . . . {Inter-connecting multiple cold equipments within or downstream of the cold box}
1/0272 . . . . {Multiple identical heat exchangers in parallel}
1/0274 . . . . {Retrofitting or revamping of an existing liquefaction unit}
1/0275 . . . . {adapted for special use of the liquefaction unit, e.g. portable or transportable devices}
1/0276 . . . . {Laboratory or other miniature devices}
1/0277 . . . . {Offshore use, e.g. during shipping}
1/0278 . . . . {Unit being stationary, e.g. on floating barge or fixed platform}
1/0279 . . . . {Compression of refrigerant or internal recycle fluid, e.g. kind of compressor, accumulator, suction drum etc.}
1/0281 . . . . {characterised by the type of prime driver, e.g. hot gas expander}
1/0282 . . . . {Steam turbine as the prime mechanical driver}
1/0283 . . . . {Gas turbine as the prime mechanical driver}
1/0284 . . . . {Electrical motor as the prime mechanical driver}
1/0285 . . . . {Combination of different types of drivers mechanically coupled to the same refrigerant compressor, possibly split on multiple compressor casings}
1/0287 . . . . {including an electrical motor}
1/0288 . . . . {using work extraction by mechanical coupling of compression and expansion of the refrigerant, so-called companders}
1/0289 . . . . {Use of different types of prime drivers of at least two refrigerant compressors in a cascade refrigeration system}
1/029 . . . . {Mechanically coupling of different refrigerant compressors in a cascade refrigeration system to a common driver}
1/0291 . . . . {Refrigerant compression by combined gas compression and liquid pumping}
1/0292 . . . . {Refrigerant compression by cold or cryogenic suction of the refrigerant gas}
1/0294 . . . . {Multiple compressor casings/strings in parallel, e.g. split arrangement}
1/0295 . . . . {Shifting of the compression load between different cooling stages within a refrigerant cycle or within a cascade refrigeration system}
1/0296 . . . . {Removal of the heat of compression, e.g. within an inter- or after-stage-cooler against an ambient heat sink}
1/0297 . . . . {using an externally chilled fluid, e.g. chilled water}
1/0298 . . . . {Safety aspects and control of the refrigerant compression system, e.g. anti-surge control}

3/00 Processes or apparatus for separating the constituents of gaseous (or liquefied gaseous) mixtures involving the use of liquefaction or solidification

3/02 . . . . by rectification, i.e. by continuous interchange of heat and material between a vapour stream and a liquid stream (F25J 3/08 takes precedence ; purification of hydrocarbons in general C07C 7/00)}
3/0204 . . . . {characterised by the feed stream (for air F25J 3/04)}
3/0209 . . . . {Natural gas or substitute natural gas}
3/0214 . . . . {Liquefied natural gas}
3/0219 . . . . {Refinery gas, cracking gas, coke oven gas, gaseous mixtures containing aliphatic unsaturated CnHm or gaseous mixtures of undefined nature}
3/0223 . . . . {H2/CO mixtures, i.e. synthesis gas; Water gas or shifted synthesis gas (production of carbon monoxide containing gas in general C01B 32/40, C10J, C10K; production of hydrogen containing gas C01B 3/00)}
3/0228 . . . . {characterised by the separated product stream}
3/0233 . . . . {separation of CnHm with 1 carbon atom or more}
3/0238 . . . . {separation of CnHm with 2 carbon atoms or more}
3/0242 . . . . {separation of CnHm with 3 carbon atoms or more}
3/0247 . . . . {separation of CnHm with 4 carbon atoms or more}
3/0252 . . . . {separation of hydrogen (production of hydrogen containing gas in general C01B 3/00, e.g. separation of hydrogen or hydrogen containing gases form gaseous mixtures at low temperatures C01B 3/006)}
3/0257 . . . . {separation of nitrogen (from air F25J 3/04, production of nitrogen in general C01B 21/00)}
3/0261 . . . . {separation of carbon monoxide (production of carbon monoxide containing gas in general C01B 32/40, C10J, C10K)}
3/0266 . . . . {separation of carbon dioxide (production of carbon dioxide in general C01B 32/00)}
3/0271 . . . . {separation of H2/CO mixtures, i.e. of synthesis gas (production of carbon monoxide containing gas in general C01B 32/40, C10J, C10K, production of hydrogen containing gas C01B 3/00)}
3/0276 . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . . .}
produced within the air fractionation unit and
{ using the cold from cryogenic liquids

different phases }
{ using the heat generated by mixing two
precedence ) }
{ using at least a triple pressure main
and F25J 3/04715
{ using a dual pressure main column system
and take precedence ) }
F25J 3/04636
{ using a single pressure main column
system only (F25J 3/0446, F25J 3/04624,
F25J 3/04636 take precedence) }
F25J 3/04460
{ using a dual pressure main column system
(F25J 3/0446, F25J 3/04624, F25J 3/04636 and
F25J 3/04715 take precedence) }
F25J 3/04412
{ in a classical double column flowsheet, i.e.
with thermal coupling by a main reboiler-
condenser in the bottom of low pressure
respectively top of high pressure column
}'}
3/04618 . . . . . . . (for cooling an air stream fed to the air fractionation unit)
3/04624 . . . . . . . [using integrated mass and heat exchange, so-called non-adiabatic rectification, e.g. dephlegmator, reflux exchanger]
3/0463 . . . . . . . (Simultaneously between rectifying and stripping sections, i.e. double dephlegmator)
3/04636 . . . . . . . [using a hybrid air separation unit, e.g. combined process by cryogenic separation and non-cryogenic separation techniques (F25J 3/04733 and F25J 3/04737 take precedence)]
3/04642 . . . . . . . [Recovering noble gases from air (from gas mixtures other than air F25J 3/028 or F25J 3/0685)]
3/04648 . . . . . . . [argon]
3/04654 . . . . . . . [Producing crude argon in a crude argon column]
3/0466 . . . . . . . (as a parallel working rectification column or auxiliary column system in a single pressure main column system)
3/04666 . . . . . . . (as a parallel working rectification column of the low pressure column in a dual pressure main column system)
3/04672 . . . . . . . [having a top condenser]
3/04678 . . . . . . . [cooled by oxygen enriched liquid from high pressure column bottoms]
3/04684 . . . . . . . [and a bottom re-boiler (F25J 3/04696 takes precedence)]
3/0469 . . . . . . . [and an intermediate re-boiler/condenser (F25J 3/04696 takes precedence)]
3/04696 . . . . . . . [a bottom re-boiler and an intermediate re-boiler/condenser]
3/04703 . . . . . . . [being arranged in more than one vessel]
3/04709 . . . . . . . [as an auxiliary column system in at least a dual pressure main column system]
3/04715 . . . . . . . [The auxiliary column system simultaneously produces oxygen]
3/04721 . . . . . . . [Producing pure argon, e.g. recovered from a crude argon column]
3/04727 . . . . . . . [using an auxiliary pure argon column for nitrogen rejection (F25J 3/04739 takes precedence)]
3/04733 . . . . . . . [using a hybrid system, e.g. using adsorption, permeation or catalytic reaction]
3/04739 . . . . . . . [in combination with an auxiliary pure argon column]
3/04745 . . . . . . . [Krypton and/or Xenon]
3/04751 . . . . . . . [Producing pure krypton and/or xenon recovered from a crude krypton/xenon mixture]
3/04757 . . . . . . . [using a hybrid system, e.g. using adsorption, permeation or catalytic reaction]
3/04763 . . . . . . . [Start-up or control of the process; Details of the apparatus used]
3/04769 . . . . . . . [Operation, control and regulation of the process; Instrumentation within the process]
3/04775 . . . . . . . [Air purification and pre-cooling]
3/04781 . . . . . . . [Pressure changing devices, e.g. for compression, expansion, liquid pumping]
3/04787 . . . . . . . [Heat exchange, e.g. main heat exchange line; Subcooler, external reboiler-condenser (F25J 3/04793 and F25J 3/0486 takes precedence)]
3/04793 . . . . . . . [Rectification, e.g. columns; Reboiler-condenser (F25J 3/0486 takes precedence)]
3/048 . . . . . . . [Argon recovery]
3/04806 . . . . . . . [High purity argon purification]
3/04812 . . . . . . . [Different modes, i.e. "runs" of operation (F25J 3/04472 takes precedence)]
3/04818 . . . . . . . [Start-up of the process]
3/04824 . . . . . . . [Stopping of the process, e.g. defrosting or derimming; Back-up procedures]
3/0483 . . . . . . . [Rapid load change of the air fractionation unit]
3/04836 . . . . . . . [Variable air feed, i.e. "load" or product demand during specified periods, e.g. during periods with high respectively low power costs (F25J 3/0483 takes precedence)]
3/04842 . . . . . . . [Intermittent process, so-called batch process]
3/04848 . . . . . . . [Control strategy, e.g. advanced process control or dynamic modeling]
3/04854 . . . . . . . [Safety aspects of operation]
3/0486 . . . . . . . [of vaporisers for oxygen enriched liquids, e.g. purging of liquids]
3/04866 . . . . . . . [Construction and layout of air fractionation equipments, e.g. valves, machines (F25J 5/00 takes precedence)]
3/04872 . . . . . . . [Vertical layout of cold equipments within in the cold box, e.g. columns, heat exchangers etc.]
3/04878 . . . . . . . [Side by side arrangement of multiple vessels in a main column system, wherein the vessels are normally mounted one upon the other or forming different sections of the same column (multiple vessels of a crude argon column F25J 3/04703)]
3/04884 . . . . . . . [Arrangement of reboiler-condensers]
3/0489 . . . . . . . [Modularity and arrangement of parts of the air fractionation unit, in particular of the cold box, e.g. pre-fabrication, assembling and erection, dimensions, horizontal layout "plot" (F25J 3/0482 takes precedence)]
3/04896 . . . . . . . [Details of columns, e.g. internals, inlet/outlet devices]
3/04903 . . . . . . . [Plates or trays]
3/04909 . . . . . . . [Structured packings]
3/04915 . . . . . . . [Combinations of different material exchange elements, e.g. within different columns]
3/04921 . . . . . . . [within the same column]
3/04927 . . . . . . . [Liquid or gas distribution devices]
3/04933 . . . . . . . [Partitioning walls or sheets]
3/04939 . . . . . . . [Vertical, e.g. dividing wall columns (details of dephlegmators F25J 5/007)]
3/0495 . . . . . {Details of internal structure; insulation and housing of the cold box}
3/0491 . . . . . {Arrangements of multiple air fractionation units or multiple equipments fulfilling the same process step, e.g. multiple trains in a network} (F25J 3/04636 takes precedence)
3/04957 . . . . . {and inter-connecting equipments upstream of the fractionation unit (s), i.e. at the “front-end”}
3/04963 . . . . . {and inter-connecting equipment within or downstream of the fractionation unit(s) (F25J 3/04393 takes precedence)
3/04969 . . . . . [Retrofitting or revamping of an existing air fractionation unit]
3/04975 . . . . . [adapted for special use of the air fractionation unit, e.g. transportable devices by truck or small scale use]
3/04981 . . . . . [for portable medical or home use]
3/04987 . . . . . [for offshore use]
3/04993 . . . . . [for space applications, e.g. for rocket use]
3/06 . by partial condensation (F25J 3/08 takes precedence; by rectification F25J 3/02 (purification of hydrocarbons in general C07C 7/00))
3/0605 . . . . . {characterised by the feed stream (for air F25J 3/04)]
3/061 . . . . . [Natural gas or substitute natural gas]
3/0615 . . . . . [Liquefied natural gas]
3/062 . . . . . [Refinery gas, cracking gas, coke oven gas, gaseous mixtures containing aliphatic unsaturated CnHm or gaseous mixtures of undefined nature]
3/0625 . . . . . [H2/CO mixtures, i.e. synthesis gas; Water gas or shifted synthesis gas (production of carbon monoxide containing gas in general C01B 3/00, C10J, C10K; production of hydrogen containing gas C01B 3/00)]
3/063 . . . . . [characterised by the separated product stream]
3/0635 . . . . . [separation of CnHm with 1 carbon atom or more]
3/064 . . . . . [separation of CnHm with 2 carbon atoms or more]
3/0645 . . . . . [separation of CnHm with 3 carbon atoms or more]
3/065 . . . . . [separation of CnHm with 4 carbon atoms or more]
3/0655 . . . . . [separation of hydrogen (production of hydrogen containing gas in general C01B 3/00, e.g. separation of hydrogen or hydrogen containing gases form gaseous mixtures at low temperatures C01B 3/00)]
3/066 . . . . . [separation of nitrogen (from air F25J 3/04, production of nitrogen in general C01B 2/00)]
3/0665 . . . . . [separation of carbon monoxide (production of carbon monoxide containing gas in general C01B 3/00, C10J, C10K)]
3/067 . . . . . [separation of carbon dioxide (production of carbon dioxide in general C01B 3/00)]
3/0675 . . . . . [separation of H2/CO mixtures, i.e. of synthesis gas (production of carbon monoxide containing gas in general C01B 3/00, C10J, C10K, production of hydrogen containing gas C01B 3/00)]
3/068 . . . . . [separation of H2/N2 mixtures, i.e. of ammonia synthesis gas (in general C01B 3/00)]
3/0685 . . . . . [separation of noble gases (from air F25J 3/0642; in general C01B 23/00)]
3/069 . . . . . [of helium]
3/0695 . . . . . [Start-up or control of the process; Details of the apparatus used]
3/08 . Separating gaseous impurities from gases or gaseous mixtures (or from liquefied gases or liquefied gaseous mixtures) (cold traps B01D 8/00)
5/00 Arrangements of cold exchangers or cold accumulators in separation or liquefaction plants (heat exchangers F28C, F28D, F28F)
5/002 . [for continuously recuperating cold, i.e. in a so-called recuperative heat exchanger]
5/005 . [in a reboiler-condenser, e.g. within a column]
5/007 . [combined with mass exchange, i.e. in a so-called dephlegmator]
Processes characterised by the type or other details of the feed stream

- Multiple feed streams, e.g. originating from different sources
- Mixing or blending of fluids with the feed stream
- Splitting of the feed stream, e.g. for treating or cooling in different ways
- Refinery or petrochemical off-gas

Processes characterised by the type or other details of the product stream

- Mixing or blending of fluids to yield a certain product
- Recovery of liquid products
- Hydrogen
- Carbon monoxide
- HYCO synthesis gas, e.g. H₂/CO mixture
- Ammonia synthesis gas, e.g. H₂/N₂ mixture
- Helium
- Neon
- Xenon
- Air or oxygen enriched air, i.e. generally less than 30mol% of O₂
- Nitrogen or special cases, e.g. multiple or low purity N₂
- Ultra high purity nitrogen, i.e. generally less than 1 ppb impurities
- Oxygen or special cases, e.g. isotope-mixtures or low purity O₂
- Oxygen production with multiple purity O₂
- Oxygen production with multiple pressure O₂
- Ultra high purity oxygen, i.e. generally more than 99,9% O₂
- Argon
- Methane
- Ethane or ethylene
- Propane or propylene
- Butane or mixed butanes
- Carbon dioxide

Processes involving steps for the removal of impurities

- Separating impurities in general from the feed stream
- Separating impurities in general from the product stream
- Separating high boiling, i.e. less volatile components from air, e.g. CO₂, hydrocarbons
- Separating low boiling, i.e. more volatile components from nitrogen, e.g. He, H₂, Ne
- Separating high boiling, i.e. less volatile components from nitrogen, e.g. CO, Ar, O₂, hydrocarbons
Processes or apparatus involving steps for increasing the pressure of gaseous process streams

Processes or apparatus involving steps for recycling of process streams

Processes or apparatus involving steps for separating reactants from products

Processes or apparatus involving steps for separating low boiling, i.e. more volatile components from oxygen, e.g. N₂, Ar

Processes or apparatus involving steps for separating high boiling, i.e. less volatile components from oxygen, e.g. Kr, Xe, Hydrocarbons, Nitrous oxides, O₂

Processes or apparatus involving steps for separating impurities from natural gas, e.g. mercury, cyclical hydrocarbons

Processes or apparatus involving steps for separating low boiling components, e.g. He, H₂, N₂, Air

Processes or apparatus involving steps for separating heavy hydrocarbons, e.g. NGL, LPG, C₄+ hydrocarbons or heavy condensates in general

Processes or apparatus involving steps for separating acid gases, e.g. CO₂, SO₂, H₂S or RSH

Processes or apparatus involving steps for separating water or hydrates

Processes or apparatus involving steps for separating impurities from carbon dioxide, e.g. H₂O or water-soluble contaminants

Processes or apparatus involving steps for separating low boiling, i.e. more volatile components, e.g. He, H₂, CO, Air gases, CH₄

Processes or apparatus involving steps for separating high boiling, i.e. less volatile components, e.g. NOₓ, SOₓ, H₂S

Processes or apparatus involving steps for separating isotopes of a component, e.g. H₂, O₂

Processes or apparatus involving steps for processes or apparatus involving steps for expanding of process streams

Processes or apparatus involving steps for recycling of process streams

Processes or apparatus involving steps for separating high boiling, i.e. less volatile components from oxygen, e.g. Kr, Xe, Hydrocarbons, Nitrous oxides, O₂

Processes or apparatus involving steps for separating impurities from natural gas, e.g. mercury, cyclical hydrocarbons

Processes or apparatus involving steps for separating low boiling components, e.g. He, H₂, N₂, Air

Processes or apparatus involving steps for separating heavy hydrocarbons, e.g. NGL, LPG, C₄+ hydrocarbons or heavy condensates in general

Processes or apparatus involving steps for separating acid gases, e.g. CO₂, SO₂, H₂S or RSH

Processes or apparatus involving steps for separating water or hydrates

Processes or apparatus involving steps for separating impurities from carbon dioxide, e.g. H₂O or water-soluble contaminants

Processes or apparatus involving steps for separating low boiling, i.e. more volatile components, e.g. He, H₂, CO, Air gases, CH₄

Processes or apparatus involving steps for separating high boiling, i.e. less volatile components, e.g. NOₓ, SOₓ, H₂S

Processes or apparatus involving steps for separating isotopes of a component, e.g. H₂, O₂

Processes or apparatus involving steps for processes or apparatus involving steps for expanding of process streams

Processes or apparatus involving steps for recycling of process streams

Processes or apparatus involving steps for separating reactants from products

Processes or apparatus involving steps for separating low boiling, i.e. more volatile components from oxygen, e.g. N₂, Ar

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Refugeation techniques used

- Coupling of processes or apparatus to other units; Integrated schemes
  - Integration in an installation for exchanging heat, e.g. for waste heat recovery
  - Integration in a gas transmission system at a pressure reduction, e.g. "let down" station
  - Integration in an installation for liquefying or solidifying a fluid stream
  - Integration in an installation using renewable energy
  - Integration in an installation using nitrogen, e.g. as utility gas, for inerting or purging purposes in IGCC, POX, GTL, PSA, float glass forming, incineration processes, for heat recovery or for enhanced oil recovery
- Using nitrogen for cooling purposes
- Using nitrogen for cooling purposes

Refrigeration techniques used

- Internal refrigeration with liquid vaporising loop
- Internal refrigeration with work-producing gas expansion loop
- with multiple gas expansion loops
- Internal refrigeration by flash gas recovery expansion loop
- External refrigeration with liquid vaporising loop
- External refrigeration with work-producing gas expansion loop
- with multiple gas expansion loops of the same refrigerant
- External refrigeration with incorporated cascade loop
- Quasi-closed internal or closed external hydrogen refrigeration cycle
- Quasi-closed internal or closed external carbon monoxide refrigeration cycle
- Quasi-closed internal or closed external helium refrigeration cycle
- Quasi-closed internal or closed external air refrigeration cycle
- Quasi-closed internal or closed external nitrogen refrigeration cycle
- Quasi-closed internal or closed external oxygen refrigeration cycle
- Quasi-closed internal or closed external argon refrigeration cycle
- Closed external refrigeration cycle with single component refrigerant (SCR), e.g. C1-, C2- or C3-hydrocarbons
- Closed external refrigeration cycle with multi component refrigerant (MCR), e.g. mixture of hydrocarbons
- Quasi-closed internal or closed external carbon dioxide refrigeration cycle
- Quasi-closed internal refrigeration or heat pump cycle, if not otherwise provided
- External refrigeration, e.g. conventional closed-loop mechanical refrigeration unit using Freon or NH₃, unspecified external refrigeration

Control of the process or apparatus

- Control of the process or apparatus
- Control for general, load changes, different modes ("runs"), measurements
- Control for or during start-up and cooling down of the installation
- Control for stopping, deriming or defrosting after an emergency shut-down of the installation or for back up system
- Control of a discontinuous or intermittent ("batch") process
- Control of freezing of components
- Advanced process control, e.g. adaptive or multivariable control

Other details not covered by groups

- Other details not covered by groups
- Comparison of processes or apparatuses
- Mathematical formulae, modeling, plot or curves; Design methods
- Particular process parameters like pressure, temperature, ratios
- Particular dimensions; Small scale or microdevices
- Details about heat insulation or cold insulation
- Details on header or distribution passages of heat exchangers, e.g. of reboiler-condenser or plate heat exchangers
- Details about subcoaling of liquids
- Vertical layout or arrangement of cold equipments within in the cold box, e.g. columns, condensors, heat exchangers etc.
- Modularity, pre-fabrication of modules, assembling and erection, horizontal layout, i.e. plot plan, and vertical arrangement of parts of the cryogenic unit, e.g. of the cold box
- Materials used, e.g. copper, steel or alloys thereof or surface treatments used, e.g. enhanced surface
- Arrangement of multiple equipments fulfilling the same process step in parallel
- Details about pipelines, i.e. network, for feed or product distribution
- Details of storing a fluid in a tank
- Processing device is mobile or transportable, e.g. by hand, car, ship, rocket engine etc.
- Processing device is used off-shore, e.g. on a platform or floating on a ship or barge
- Retrofitting, revamping or debottlenecking of existing plant
- Details about safety operation of the installation